

WHAT IS CLAIMED IS:

1. A process for purification of dipeptide sweeteners and dipeptide derivative sweeteners, comprising the steps of:
 - (a) feeding a slurry comprising dipeptide sweetener or dipeptide derivative sweetener crystals to a filter unit comprising at least one filter element selected from the group comprising sintered metal filter elements and porous ceramic filter elements, said slurry being fed to the inside of said filter element;
 - (b) providing sufficient pressure to said filter unit to force liquid from said slurry through said filter element;
 - (c) removing said liquid from said filter unit;
 - (d) recovering the remaining portion of said slurry, comprising crystals of said dipeptide sweetener or dipeptide derivative sweetener.
2. The process of Claim 1 wherein said sintered metal filter element is from two-inches to four-inches in diameter and thirty to fifty inches tall.
3. The process of Claim 1 wherein said sintered metal filter element has a pore size of about 0.5-15 microns.
4. The process of Claim 1 wherein said slurry comprises 0.1 to 10% aspartame by weight.
5. The process of Claim 4 wherein said slurry comprises 5 to 6% aspartame by weight.
6. The process of Claim 1 wherein said slurry is fed to the inside of the filter element via a valve located at the bottom of said filter unit.
7. The process of Claim 1 wherein said pressure in step (b) is in the range of 5 to 120 psi.
8. The process of Claim 7 wherein said pressure in step (b) is in the range of 40 to 80 psi.
9. The process of Claim 1 comprising the additional step between steps (c) and (d):

supplying pressurized air to the bottom of said filter unit, said pressurized air being vented from the top of said filter unit to remove additional water from said filter unit.

10. A process for purification of dipeptide sweeteners and dipeptide derivative sweeteners, comprising the steps of:
 - (a) feeding a slurry comprising dipeptide sweetener or dipeptide derivative sweetener crystals to a filter unit comprising at least one filter element selected from the group comprising sintered metal filter elements and porous ceramic filter elements, said slurry being fed to the inside of said filter element;
 - (b) providing sufficient flow rate to said filter unit to force liquid from said slurry through said filter element;
 - (c) supplying pressurized air to the bottom of said filter unit, said pressurized air being vented from the vent and body drain of said filter unit to remove additional water from said filter unit to form a solid cake comprising crystals of dipeptide or dipeptide derivative sweetener;
 - (d) supplying cold water to the bottom of said filter unit, said water passing through said cake and filter element and being discharged from said filter body drain, resulting in the removal of impurities from said solid cake;
 - (e) forcing pressurized water followed by pressurized air through said cake for the purpose of compacting and removing excess water from said cake;
 - (f) forcing heated air through said cake for the purpose of dehydrating said compacted cake;
 - (g) discharging said dehydrated compacted cake by pressurizing said filter unit and opening a valve in said unit.
11. The process of Claim 10 wherein said sintered metal filter element is from about two inches to four inches in diameter and thirty to fifty inches in height.

12. The process of Claim 10 wherein said sintered metal filter element has a pore size of about 0.5 –15 microns.
13. The process of Claim 1 wherein said slurry comprises 0.1 to 10% aspartame by weight.
14. The process of Claim 4 wherein said slurry comprises 5 to 6% aspartame by weight.
15. The process of Claim 1 wherein said slurry is fed to the inside of the filter element via a valve located at the bottom of said filter unit.
16. The process of Claim 1 wherein the flow rate in step (b) is about 0.5 to 5 liters per minute per square foot of element surface.
17. The process of Claim 16 wherein said flow rate in step (b) is about 3 liters per minute per square foot of element surface.
18. The process of Claim 10 wherein said flow rate of said cold water in step (d) is about 3.5 liters per minute per square foot of element surface.
19. The process of Claim 10 wherein said flow rate of said compressed air in step (e) is in excess of 7 standard cubic feet per minute per square foot of element for a period of at least one minute.
20. The process of Claim 10 wherein the volume of pressurized water in step (e) is about 0.3 to 5 liters per square foot of element surface.
21. The process of Claim 20 wherein said volume of pressurized water in step (e) is about 2 liters per minute per square foot of element surface.

22. The process of Claim 21 wherein said volume of pressurized water in step (e) is applied for at least 30 seconds.
23. The process of Claim 10 wherein the volume of pressurized air in steps (e) and (f) is about 1.5 to 15 standard cubic feet per minute per square foot of element.
24. The process of Claim 23 wherein said volume of pressurized air in steps (e) and (f) is about 7 standard cubic feet per minute per square foot of element.
25. The process of Claim 24 wherein said volume of pressurized air in steps (e) and (f) is applied for at least five minutes.
26. The process of Claim 24 wherein said pressurized air is applied until said cake has a moisture level of between 20-35% by weight.
27. The process of Claim 10 wherein the air applied in step (f) is in the range of 32-150°C.
28. The process of Claim 10 wherein step (f) is carried out under heat conditions whereby the air temperature in said element is between 230-260° C.
29. The process of Claim 10 wherein step (g) wherein said filter unit is pressurized to a pressure of between about 30-100 psi.